

I certify that the work being submitted is my own, and that no unauthorized assistance was obtained.

Name (please print): _____

Signature: _____

Exam #2

(Closed book, closed notes)

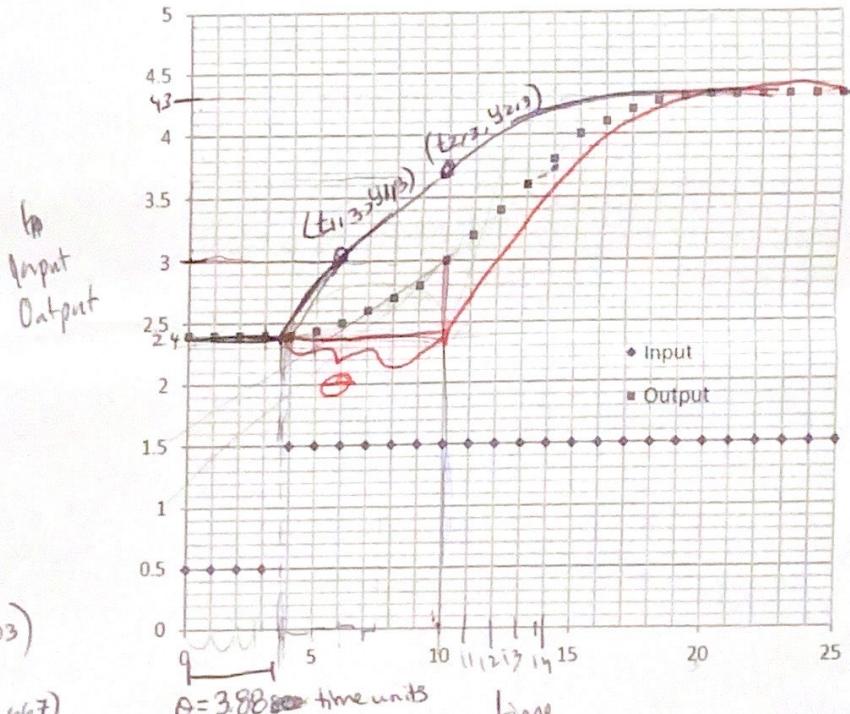
1. For the experimental data below:

- (a) Develop a first order plus dead time (FOPDT) model for the input-output system shown below. (10 pts) **10**
- (b) Sketch your model prediction of the output on the axes by showing the main model parameters on the graph. (10 pts) **5**
- (c) Can you determine the order of the process system generating this output? Explain your answer. (5 pts) **0**

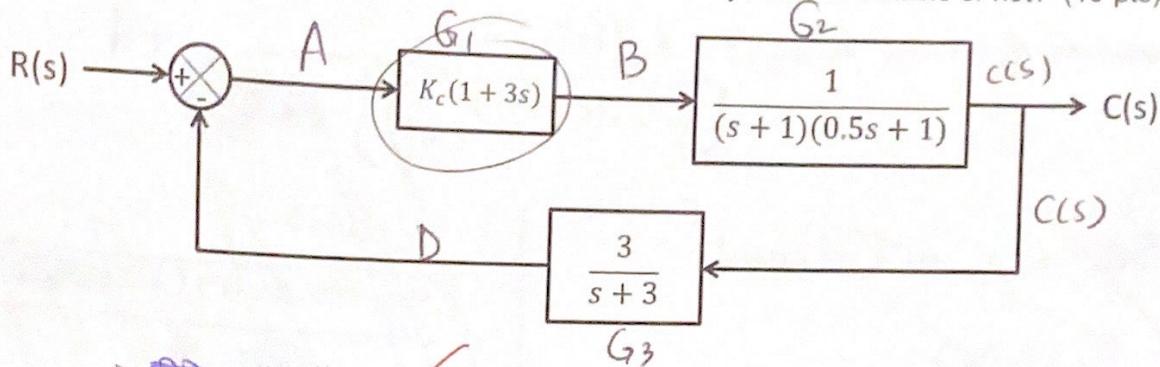
16
 $(t_{113}, y_{113}) = (6, 3.03)$

$$(t_{213}, y_{213}) = (9.7, 3.667)$$

$\theta = 3.88$ seconds time units (deadtime)



- 35 The block diagram below illustrates a feedback control system for a controlled variable $C(s)$
- What kind of controller or control algorithm is being used in this system? (5 pts) **5**
 - Develop the overall transfer function $C(s)/R(s)$. (5 pts) **5**
 - Determine the final value of $C(t)$ if K_c is 9 and $R(t)$ exhibits a step change of +12 units. (10 pts) **10**
 - Evaluate the stability of this process feedback control system. Is it stable or not? (15 pts) **15**



a) PD controller ✓

$$P \rightarrow K_c$$

$$D \rightarrow T(s) \text{ term}$$

There is no $\frac{1}{s}$ term, so no I controller

$$b) \frac{C(s)}{R(s)} =$$

$$\frac{C(s)}{R(s)} = \frac{\text{multiply straight through } R(s) \text{ to } C(s)}{\text{multiply loop} + 1}$$

$$= \frac{G_1 G_2}{G_1 G_2 G_3 + 1}$$

$$c) K_c = 9$$

$$R(t) = 12$$

$$R(s) = \frac{12}{s}$$

$$FVT \rightarrow \lim_{s \rightarrow 0} [s(F(s))] = \lim_{t \rightarrow \infty} [f(t)]$$

$$F(s) \Rightarrow \frac{G_1 G_2}{G_1 G_2 G_3 + 1} * R(s) \frac{12}{s}$$

$$\Rightarrow K_c(1+3s) \left(\frac{1}{s+1} \right) \left(\frac{1}{0.5s+1} \right) \left(\frac{3}{s+3} \right) + 1$$

$$\begin{aligned} & \lim_{s \rightarrow 0} \left(\frac{K_c(1+3s)}{s+1} \frac{1}{0.5s+1} \frac{3}{s+3} + 1 \right) \cdot \frac{12}{s} \\ &= \frac{9 * 12}{9+1} \Rightarrow \boxed{10.8} \end{aligned}$$

$$\frac{9(1)}{(1)(1)} \left(\frac{1}{1+1} \right) \left(\frac{3}{3} \right) + 1$$

d) Stability

$\frac{C(s)}{R(s)}$ take denominator to assess stability with Routh Array ~~and~~

Denominator of transfer function: $K_C(1+3s)$

Set $= 0$ and expand

$$K_C(1+3s)$$

$$(S+1)(0.5S+1)\left(\frac{3}{S+3}\right) + 1 = 0$$

$$K_C + 3K_C s$$

$$\frac{3(0.5S^2 + 3S + 3) + 3(0.5S) + 3}{S+3} = 0$$

$$\frac{9K_C + 9K_C s}{S+3} + 1.5S^2 + 3S + 1.5S + 3 + S + 3 = 0$$

$$S+3$$

$$R \quad 9 + 27s$$

$$\frac{9(1.5S^2 + 3S + 1.5S + 3) + 3(3S) + 3^2 + 3S}{S+3} = 0$$

$$\frac{4.5S^3 + 9S^2 + 4.5S^2 + 9S + 3S^2 + 9S}{16.5} = 0$$

2 criteria:
The whole first column of the array is positive so the system is stable

$$\frac{(3)(86.5) - (0.5)(30)}{3}$$

$$\begin{array}{cccc} K_C(1+3s) & & & \\ (S+1)(0.5S+1)(3) & & & \\ S+3 & & & \\ S+3 = K_C(1+3s) & & & \\ (S+1)(0.5S+1)(3) & & & \end{array} = -1$$

$$\frac{K_C(1+3s)(3)}{(S+3)(0.5S+1)(S+1)} = -1 \checkmark$$

$$\frac{9K_C + 9K_C s}{0.5S+1} = -S^2 \pm 4S \pm 3$$

$$\frac{9K_C + 9K_C s}{-S^2 \pm 4S \pm 3} = 0.5S^3 - 2S^2 - 1.5S$$

$$\frac{36 + 108s}{27 + 81s} = 0.5S^3 - 3S^2 \pm 5.5S \pm 3$$

~~$$-\frac{3}{5}S^3 - \frac{2}{5}S^2 - \frac{75}{2}S - 24$$~~

~~$$① 0.5S^3 + 3S^2 + 86.5S + 30 = 0$$~~

all coefficients are positive
satisfies first criteria for stability

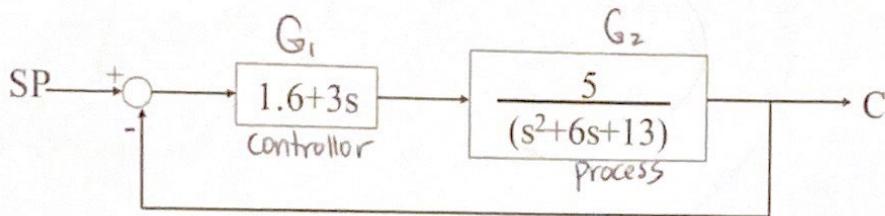
② Routh array:

$a_3/3$	a_1	86.5
$a_2/3$	a_0	30
$\frac{a_2 a_1 - a_3 a_0}{a_2}$	0	0
$a_0/30$	0	0

$$a_3 = 0.5 \quad a_1 = 86.5$$

$$a_2 = 3 \quad a_0 = 30$$

3. The set point (SP) of the control system below is given a step change of 0.2 units.
- (a) The blocks shown represent a process system and a controller. Identify as many parameters of the process system as you can and explain what type of open loop behavior you would expect for the system to display for a direct step change input. (5 pts) **5**
- (b) Determine the final value of C after the setpoint change. (10 pts) **10**
- (c) Describe the closed loop dynamic behavior of C after the set point change. (15 pts) **10**
- (d) Calculate the offset in C after the setpoint change. (15 pts) **0**
- (e) If you wished to sabotage the operation of this system by altering the controller settings to produce unstable behavior after a 0.2 unit setpoint change, how would you do it? Describe with supporting numbers. (15 pts) **15**
- 40**



$$\text{Transfer function} = \frac{\text{output}}{\text{input}} = \frac{C(s)}{SP(s)} = \frac{G_1 G_2}{G_1 G_2 + 1}$$

1.6 + 3s is the controller

This does not have $\frac{1}{s}$ ~~term~~

absent terms, so it is a PD controller ✓

$$K_c(1 + T_{D}s) \Rightarrow 1.6 + 3s$$

~~Kc~~ $K_c = 1.6, T_D = 1.875$ Parameters for G_1 (controller)

$$1.6(1 + 1.875s)$$

The process is a second order process ~~and~~ because of the order of s in the denominator →

$$\frac{5}{s^2 + 6s + 13}$$

$$\frac{5/13}{s^2 + 6s/13 + 1/13}$$

$$K_p = 5/13$$

$$T_p^2 s^2 = \frac{1}{13} s^2$$

$$T_p^2 = \frac{1}{13}$$

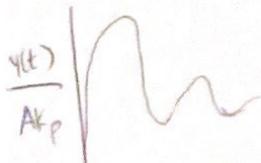
$$T_p = \sqrt{1/13}$$

Parameters for G_2

process parameters

~~1.6 + 3s~~

Bp



$$\frac{t}{T_n}$$

$\zeta < 1$ → the open loop behavior of the process will be underdamped.
There will be exponentially decreasing oscillations.

$$2\zeta T_p s = \frac{6}{13} s$$

$$2\zeta \left(\frac{1}{\sqrt{1/13}}\right) s = \frac{6}{13}$$

$$\zeta \approx 0.83$$

$$G_p(s) = \frac{K_p e^{-\theta_p s}}{T_p s + 1}$$

Neha
 $\frac{91}{105}$

$$T_p = \frac{t_{213} - t_{113}}{0.7}$$

$$\theta_p = t_{113} - 0.4 T_p$$

$$K_p = \frac{\Delta y}{\Delta u} = \frac{y(25) - y(0)}{u(25) - u(0)} = \frac{4.3 - 2.4}{1.5 - 0.5} = 1.9 \checkmark$$

~~ACB224H~~

$$y_{213} = \frac{2}{3} \Delta y + 2.4 = 3.6667$$

$$y_{113} = \frac{1}{3} \Delta y + 2.4 = 3.03$$

$$\Delta y = 4.3 - 2.4 = 1.9$$

$$t_{113} = 10 \quad (\text{time @ } y_{113}) - 4 \quad (\text{time where step function began}) = 6$$

$$t_{213} = 13.7 \quad (\text{time @ } y_{213}) - 4 = 9.7$$

$$T_p = \frac{t_{213} - t_{113}}{0.7} = \frac{9.7 - 6}{0.7} = 5.2857 \checkmark$$

$$\theta_p = t_{113} - 0.4 T_p = 6 - 0.4(5.28) = 3.88 \checkmark$$

a)

$$\therefore G_p(s) = \frac{K_p e^{-\theta_p s}}{T_p s + 1} = \frac{1.9 e^{-3.88 s}}{5.28 s + 1} \checkmark$$

b) On graph (exam page)

c) 4th order because deadline ≈ 4 (3.88)

~~4th order because of the deadline ≈ 4~~

4th order because $\theta_p \approx 4 \times$

#3b)

$$C(s) = \left(\frac{G_1 G_2}{G_1 G_2 + 1} \right) (S_p(s))$$

$\frac{0.2}{s}$

$$S_p(t) = 0.2$$

$$S_p(s) = \frac{0.2}{s}$$

$$= \frac{0.2}{s} \left(\frac{(1.6+3s)(\frac{s}{s^2+6s+13})}{(1.6+3s)(\frac{s}{s^2+6s+13}) + 1} \right) \rightarrow F(s)$$

$$FVT \rightarrow \lim_{s \rightarrow 0} sF(s) = \lim_{t \rightarrow \infty} [f(t)]$$

$$\lim_{s \rightarrow 0} \left(8 \cdot \frac{0.2}{s} \cdot F(s) \right) = 0.2(F(s))$$

$$= \lim_{s \rightarrow 0} \left(0.2 \left(\frac{(1.6+0)(\frac{s}{0+0+13})}{(1.6+0)(\frac{s}{0+0+13}) + 1} \right) \right) \checkmark$$

$$= 0.2 \left(\frac{1.6 \cdot \frac{5}{13}}{(1.6 \cdot \frac{5}{13}) + 1} \right) = 0.2 \left(\frac{0.61538}{1.6153} \right)$$

X

$0.446152 \rightarrow 0.2$
 Final value
 $C(s)$

→ Closed loop dynamic behavior given by characteristic eqn of a closed loop system $\rightarrow G_c \cdot G_p + 1 = 0$

G_c G_p

$$G_c G_p = -1$$

$$\left(\frac{5}{s^2+6s+13} \right) (1.6+3s) = -1$$

$$\frac{8+15s}{s^2+6s+13} = -1$$

$$8+15s = -s^2-6s-13$$

$$-s^2-15s-6s-13-8=0$$

$$-s^2-21s-21=0$$

$$s^2+21s+21=0$$

$$-21 \pm \sqrt{(21)^2 - 4(1)(21)} / 2(1)$$

$$\frac{-21 \pm 18.89}{2} \quad -1.055$$

19.945

The poles of the closed loop process are both negative, thus it is a stable system.

behavior ??

g ??

$$C(s) = \left(\frac{G_1 G_2}{G_1 G_2 + 1} \right) \left(\frac{s_p(s)}{\frac{0.2}{s}} \right)$$

} after | Apply FVT →
from b), 0.446152
is final

$$C(s) = \frac{G_1 G_2}{G_1 G_2 + 1} \left(s_p(s) \right)$$

} before (no change) | Apply FVT,
~~final~~

$$\lim_{s \rightarrow 0} S(F(s)) \rightarrow S\left(\frac{1.6 \cdot s/13}{(1.6 \cdot s/13) + 1}\right) \underset{s=0}{\cancel{s=0}} \text{ offset} = s_p - \text{final value}$$

The offset is 0.446152 X

3e) I would attempt to get the roots to be positive real components.
After the setpoint change, the closed loop characteristic eqn is applied,
So that was given in part c) as:

$$G_c G_p \text{ and } +1 = 0$$

$$G_c G_p = -1$$

If K_p was reduced to $\frac{1}{20}$, increased to a very large number such as 20,
the eqn (in standard form) would be

$$20 \rightarrow K_p = 20$$

$$\frac{s^2}{13} + \frac{6s}{13} + 1$$

The d) The process eqn would be given as $\frac{260}{s^2 + 6s + 13} \rightarrow \frac{260/13}{\frac{s^2}{13} + \frac{6s}{13} + 1}$

Now when finding the poles, they would be positive

$$(1.6 + 3s) \left(\frac{260}{s^2 + 6s + 13} \right) = -1 \Rightarrow \frac{260(1.6 + 3s)}{s^2 + 6s + 13} = -1$$

$$\frac{416 + 780s}{s^2 + 6s + 13} \rightarrow 416 + 780s = -s^2 - 6s - 13$$

$$-s^2 - 786s - 429 = 0$$

$$\frac{786 \pm \sqrt{786^2 - 4(-1)(-429)}}{-2}$$

$$\frac{786 \pm \sqrt{786^2 - 4(-1)(-429)}}{-2} = 787.09$$

0.543
-786.545

This is now a positive root
which can make the system unstable.